

PCTWORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau

INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification: H01B 7/28, 3/44	A1	(11) International Publication Number: WO 97/50093 (43) International Publication Date: 31 December 1997 (31.12.97)
<p>(21) International Application Number: PCT/US97/10374</p> <p>(22) International Filing Date: 20 June 1997 (20.06.97)</p> <p>(30) Priority Data: 08/669,602 24 June 1996 (24.06.96) US</p> <p>(71) Applicant: UNION CARBIDE CHEMICALS & PLASTICS TECHNOLOGY CORPORATION [US/US]; 39 Old Ridgebury Road, Danbury, CT 06817-0001 (US).</p> <p>(72) Inventors: GROSS, Laurence, Herbert; 977 Rector Road, Bridgewater, NJ 08807 (US). MENDELSON, Alfred; 1467 East 13th Street, Brooklyn, NY 11330 (US).</p> <p>(74) Agent: WIGGINS, Karen, Johnson; Union Carbide Chemicals & Plastics Technology Corporation, 39 Old Ridgebury Road, Danbury, CT 06817-0001 (US).</p>		<p>(81) Designated States: AU, CA, CN, JP, KR, MX, European patent (AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).</p> <p>Published <i>With international search report.</i></p>
<p>(54) Title: TREE RESISTANT CABLE</p> <p>(57) Abstract</p> <p>A cable comprising one or more electrical conductors or a core of one or more electrical conductors, each conductor or core being surrounded by a layer of insulation comprising a multimodal copolymer of ethylene and one or more alpha-olefins, each alpha-olefin having 3 to 8 carbon atoms, said copolymer having a broad comonomer distribution as measured by TREF with a value for the percent of copolymer, which elutes out at a temperature of greater than 90 °C, of greater than about 5 percent; a WTGR value of less than about 20 percent; a melt index in the range of about 0.1 to about 30 grams per 10 minutes; and a density in the range of 0.880 to 0.950 gram per cubic centimeter, and being prepared by a low pressure process.</p>		

FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AL	Albania	ES	Spain	LS	Lesotho	SI	Slovenia
AM	Armenia	FI	Finland	LT	Lithuania	SK	Slovakia
AT	Austria	FR	France	LU	Luxembourg	SN	Senegal
AU	Australia	GA	Gabon	LV	Latvia	SZ	Swaziland
AZ	Azerbaijan	GB	United Kingdom	MC	Monaco	TD	Chad
BA	Bosnia and Herzegovina	GE	Georgia	MD	Republic of Moldova	TG	Togo
BB	Barbados	GH	Ghana	MG	Madagascar	TJ	Tajikistan
BE	Belgium	GN	Guinea	MK	The former Yugoslav Republic of Macedonia	TM	Turkmenistan
BF	Burkina Faso	GR	Greece	ML	Mali	TR	Turkey
BG	Bulgaria	HU	Hungary	MN	Mongolia	TT	Trinidad and Tobago
BJ	Benin	IE	Ireland	MR	Mauritania	UA	Ukraine
BR	Brazil	IL	Israel	MW	Malawi	UG	Uganda
BY	Belarus	IS	Iceland	MX	Mexico	US	United States of America
CA	Canada	IT	Italy	NE	Niger	UZ	Uzbekistan
CF	Central African Republic	JP	Japan	NL	Netherlands	VN	Viet Nam
CG	Congo	KE	Kenya	NO	Norway	YU	Yugoslavia
CH	Switzerland	KG	Kyrgyzstan	NZ	New Zealand	ZW	Zimbabwe
CI	Côte d'Ivoire	KP	Democratic People's Republic of Korea	PL	Poland		
CM	Cameroon	KR	Republic of Korea	PT	Portugal		
CN	China	KZ	Kazakhstan	RO	Romania		
CU	Cuba	LC	Saint Lucia	RU	Russian Federation		
CZ	Czech Republic	LI	Liechtenstein	SD	Sudan		
DE	Germany	LK	Sri Lanka	SE	Sweden		
DK	Denmark	LR	Liberia	SG	Singapore		
EE	Estonia						

- 1 -

TREE RESISTANT CABLE

Technical Field

This invention relates to electric power cable insulated with a polyethylene composition having an improved resistance to water trees.

Background Information

A typical electric power cable generally comprises one or more conductors, which form a cable core that is surrounded by several layers of polymeric material including a first semiconducting shield layer, an insulating layer, a second semiconducting shield layer, a metallic tape or wire shield, and a jacket.

These insulated cables are known to suffer from shortened life when installed in an environment where the insulation is exposed to water, e.g., underground or locations of high humidity. The shortened life has been attributed to the formation of water trees, which occur when an organic polymeric material is subjected to an electrical field over a long period of time in the presence of water in liquid or vapor form. The net result is a reduction in the dielectric strength of the insulation.

Many solutions have been proposed for increasing the resistance of organic insulating materials to degradation by water treeing. The most recent solutions involve the addition of polyethylene glycol, as a water tree growth inhibitor, to a heterogeneous low density polyethylene such as described in United States Patents 4,305,849; 4,612,139; and 4,812, 505. Another solution is the use of a homogeneous polyethylene per se as the organic insulating material, i.e., without the addition of a water tree growth inhibitor. See United States Patent 5,246,783. Both of these solutions appear to be steps in

- 2 -

the right direction, but there is a continuous industrial demand for improvement partially because power cable is increasingly exposed to harsher environments, and partially because consumers are more concerned with cable longevity, e.g., a service life of 30 to 40 years.

Disclosure of the Invention

An object of this invention, therefore, is to provide an insulated cable which exhibits a much improved resistance to water trees. Other objects and advantages will become apparent hereinafter.

According to the invention, an insulated cable has been discovered which meets the above object.

The cable comprises one or more electrical conductors or a core of one or more electrical conductors, each conductor or core being surrounded by a layer of insulation comprising a multimodal copolymer of ethylene and one or more alpha-olefins, each alpha-olefin having 3 to 8 carbon atoms, said copolymer having a broad comonomer distribution as measured by TREF with a value for the percent of copolymer, which elutes out at a temperature of greater than 90 degrees C, of greater than about 5 percent; a WTGR value of less than about 20 percent; a melt index in the range of about 0.1 to about 30 grams per 10 minutes; and a density in the range of 0.880 to 0.950 gram per cubic centimeter, and being prepared by a low pressure process.

Description of the Preferred Embodiment(s)

The polyethylenes of interest here are copolymers of ethylene and one or more alpha-olefins, which have a broad molecular weight distribution and a broad comonomer distribution. They also have a number of other defined characteristics. The copolymers can be multimodal, but are preferably bimodal or trimodal. A copolymer is a

- 3 -

polymer formed from the polymerization of two or more monomers and includes terpolymers, tetramers, etc. In this specification, the term " multimodal (or bimodal, trimodal, etc.) copolymer" is considered to mean a single copolymer or a blend of copolymers provided that the single copolymer and the blend are multimodal and have a broad comonomer distribution as well as other attributes.

The alpha-olefins have 3 to 8 carbon atoms. Examples of the alpha-olefins are propylene, 1-butene, 1-hexene, 4-methyl-1-pentene, and 1-octene.

As noted above, the copolymers can have a density in the range of 0.880 to 0.950 gram per cubic centimeter, and preferably have a density in the range of 0.880 to about 0.930 gram per cubic centimeter. They also can have a melt index in the range of about 0.1 to about 30 grams per 10 minutes, and preferably have a melt index in the range of about 0.5 to about 10 grams per 10 minutes. Melt index is determined in accordance with ASTM D-1238, Condition E, measured at 190 degrees C. The copolymers have a broad comonomer distribution as measured by TREF with a value for the percent of copolymer, which elutes out at a temperature of greater than 90 degrees C, of greater than about 5 percent, and preferably greater than about 10 percent. The copolymers can also have a WTGR value of less than about 20 percent, preferably less than about 10 percent, and most preferably less than about 5 percent. TREF and WTGR are discussed below.

The polyethylenes used in subject invention are preferably produced in the gas phase by various low pressure processes. They can also be produced in the liquid phase in solutions or slurries by conventional techniques. Low pressure processes are typically run at pressures below 1000 psi whereas high pressure processes are typically run at pressures above 15,000 psi. Typical catalyst systems, which can be used to prepare these polyethylenes, are magnesium/titanium based

- 4 -

catalyst systems, which can be exemplified by the catalyst system described in United States patent 4,302,565 and a spray dried catalyst system described in United States patent 5,290,745; vanadium based catalyst systems such as those described in United States patents 4,508,842 and 4,918,038; a chromium based catalyst system such as that described in United States patent 4,101,445; metallocene catalyst systems such as those described in United States patents 5,272,236 and 5,317,036; or other transition metal catalyst systems. Many of these catalyst systems are often referred to as Ziegler-Natta catalyst systems. Catalyst systems, which use chromium or molybdenum oxides on silica-alumina supports, are also useful. Typical processes for preparing the polyethylenes are also described in the aforementioned patents. Typical in situ polyethylene blends and processes and catalyst systems for providing same are described in United States Patents 5,371,145 and 5,405,901.

As long as the blend, whether formed in situ or by mechanical means, is multimodal and has a broad comonomer distribution, the polymers can be blended in varying amounts in the range of about 1 to about 99 percent by weight.

Conventional additives, which can be introduced into the polyethylene formulation, are exemplified by antioxidants, coupling agents, ultraviolet absorbers or stabilizers, antistatic agents, pigments, dyes, nucleating agents, reinforcing fillers or polymer additives, slip agents, plasticizers, processing aids, lubricants, viscosity control agents, tackifiers, anti-blocking agents, surfactants, extender oils, metal deactivators, voltage stabilizers, flame retardant fillers and additives, crosslinking agents, boosters, and catalysts, and smoke suppressants. Fillers and additives can be added in amounts ranging from less than about 0.1 to more than about 200 parts by weight for each 100 parts by weight of the base resin, in this case, polyethylene.

- 5 -

Examples of antioxidants are: hindered phenols such as tetrakis[methylene(3,5-di-tert-butyl-4-hydroxyhydrocinnamate)]-methane, bis[(beta-(3,5-ditert-butyl-4-hydroxybenzyl)-methylcarboxyethyl)]sulphide, 4,4'-thiobis(2-methyl-6-tert-butylphenol), 4,4'-thiobis(2-tert-butyl-5-methylphenol), 2,2'-thiobis(4-methyl-6-tert-butylphenol), and thiodiethylene bis(3,5-di-tert-butyl-4-hydroxy)hydrocinnamate; phosphites and phosphonites such as tris(2,4-di-tert-butylphenyl)phosphite and di-tert-butylphenylphosphonite; thio compounds such as dilaurylthiodipropionate, dimyristylthiodipropionate, and distearylthiodipropionate; various siloxanes; and various amines such as polymerized 2,2,4-trimethyl-1,2-dihydroquinoline. Antioxidants can be used in amounts of about 0.1 to about 5 parts by weight per 100 parts by weight of polyethylene.

The resins in the formulation can be crosslinked by adding a crosslinking agent to the composition or by making the resin hydrolyzable, which is accomplished by adding hydrolyzable groups such as $-\text{Si}(\text{OR})_3$ wherein R is a hydrocarbyl radical to the resin structure through copolymerization or grafting.

Suitable crosslinking agents are organic peroxides such as dicumyl peroxide; 2,5-dimethyl-2,5-di(t-butylperoxy)hexane; t-butyl cumyl peroxide; and 2,5-dimethyl-2,5-di(t-butylperoxy)hexane-3. Dicumyl peroxide is preferred.

Hydrolyzable groups can be added, for example, by copolymerizing (in the case of the homogeneous polyethylene) ethylene and comonomer(s) with an ethylenically unsaturated compound having one or more $-\text{Si}(\text{OR})_3$ groups such as vinyltrimethoxy-silane, vinyltriethoxysilane, and gamma-methacryloxypropyltrimethoxysilane or grafting these silane compounds to the either resin in the presence of the aforementioned organic peroxides. The hydrolyzable resins are then crosslinked by moisture in the presence of a silanol condensation

- 6 -

catalyst such as dibutyltin dilaurate, dioctyltin maleate, dibutyltin diacetate, stannous acetate, lead naphthenate, and zinc caprylate. Dibutyltin dilaurate is preferred.

Examples of hydrolyzable copolymers and hydrolyzable grafted copolymers are ethylene/comonomer/ vinyltrimethoxy silane copolymer, ethylene/comonomer/gamma-methacryloxypropyltrimethoxy silane copolymer, vinyltrimethoxy silane grafted ethylene/comonomer copolymer, vinyltrimethoxy silane grafted linear low density ethylene/1-butene copolymer, and vinyltrimethoxy silane grafted low density polyethylene or ethylene homopolymer.

The cable of the invention can be prepared in various types of extruders, e.g., single or twin screw types. Compounding can be effected in the extruder or prior to extrusion in a conventional mixer such as a Brabender™ mixer ; a Banbury™ mixer; or the twin screw extruder. A description of a conventional extruder can be found in United States patent 4,857,600. A typical extruder has a hopper at its upstream end and a die at its downstream end. The hopper feeds into a barrel, which contains a screw. At the downstream end, between the end of the screw and the die, is a screen pack and a breaker plate. The screw portion of the extruder is considered to be divided up into three sections, the feed section, the compression section, and the metering section, and two zones, the back heat zone and the front heat zone, the sections and zones running from upstream to downstream. In the alternative, there can be multiple heating zones (more than two) along the axis running from upstream to downstream. If it has more than one barrel, the barrels are connected in series. The length to diameter ratio of each barrel is in the range of about 15:1 to about 30:1. In wire coating, where the material is crosslinked after extrusion, the die of the crosshead feeds directly into a heating zone, and this zone can be

- 7 -

maintained at a temperature in the range of about 130°C to about 260°C, and preferably in the range of about 170°C to about 220°C.

The advantages of the invention lie in the much improved water tree growth rate; that additives used to enhance water tree resistance can be avoided; that the "all" polyethylene composition takes full advantage of the desirable electrical characteristics of polyethylene, for example, its low dissipation factor and excellent AC breakdown strength; and the composition being useful in low, medium, and high voltage applications.

The patents mentioned in this specification are incorporated by reference herein.

The invention is illustrated by the following examples.

Examples 1 to 11

The resistance of insulating compositions to water treeing is determined by the method described in United States Patent 4,144,202. This measurement leads to a value for water tree resistance relative to a standard polyethylene insulating material. The term used for the value is "water tree growth rate" (WTGR). The lower the values of WTGR, the better the water tree resistance. The WTGR values are stated in percent.

TREF is also measured. The measurement is a technique, well recognized by those skilled in the art. The acronym stands for Temperature Rising Elution Fractionation. When more than 5 (preferably more than 10) percent by weight of the resin has an elution temperature greater than 90 degrees C, a broad comonomer distribution and a lower WTGR are indicated. Generally, the higher the TREF value, the lower the WTGR. The TREF values are stated in percent of the resin, which elutes out at greater than 90 degrees C.

100 parts by weight of each of the three copolymers of ethylene described below are compounded in a twin screw BRABENDER™

- 8 -

extruder with 0.35 part by weight of the primary antioxidant, thiodiethylene bis(3,5-di-tert-butyl-4-hydroxy)hydro-cinnamate, and 0.35 part by weight of the secondary antioxidant, distearyl thio dipropionate. The extruder is run at 60 revolutions per minute (rpm) at a 155 degree C melt temperature. A second pass in the same equipment under the same conditions is run in order to better homogenize the mixture. To this mixture (held at 75 degrees C) is added 1.7 parts dicumyl peroxide via a 125 to 130 degree C fluxing on a two roll mill to provide an oscillating disk rheometer (5 degree arc at 360 degrees F) reading of 32.9 inch-pounds of torque (COPOLYMER A), 33.8 inch-pounds of torque (COPOLYMER B), and 33.8 inch-pounds of torque (COPOLYMER C), respectively. Each composition is then removed from the two roll mill as a crepe and diced and molded into one inch discs which are 0.25 inch thick in a press in two steps:

	initial step	final step
pressure (psi)	low	high
temperature (°C)	120	175
residence time (minutes)	9	15 to 20

COPOLYMER A: This copolymer is an in situ blend of a copolymer of ethylene and 1-hexene as the high molecular weight component and a copolymer of ethylene and 1-butene as the low molecular weight component. Copolymer A is bimodal; has a density of 0.923 gram per cubic centimeter; a melt index of 0.6 gram per 10 minutes; a flow index of 77 grams per 10 minutes. Flow index is determined under ASTM D-1238, Condition F, at 190 degrees C and 21.6 kilograms.

- 9 -

COPOLYMER B: This copolymer is a 50:50 percent by weight mechanical blend of a copolymer of ethylene and 1-hexene as the high molecular weight component and a copolymer of ethylene and 1-hexene as the low molecular weight component. The high molecular weight component has a density of 0.895 gram per cubic centimeter and a flow index of 4.5 grams per 10 minutes. The low molecular weight component has a density of 0.924 gram per cubic centimeter and a melt index of 500 grams per 10 minutes. The blend is bimodal.

COPOLYMER C: This copolymer is a heterogeneous copolymer of ethylene and 1-hexene made in a low pressure process using a magnesium/titanium catalyst system. It is monomodal and has a density of 0.905 gram per cubic centimeter and a melt index of 4 grams per 10 minutes.

COPOLYMER D: This copolymer is a heterogeneous copolymer of ethylene and 1-butene made in a low pressure process using a magnesium/titanium catalyst system. It is monomodal and has a density of 0.905 gram per cubic centimeter and a melt index of 4 grams per 10 minutes.

COPOLYMER E: This copolymer is bimodal. The low molecular weight component is a copolymer of ethylene and 1-butene and the high molecular weight component is a copolymer of ethylene and 1-hexene. The bimodal copolymer has a density of 0.913 gram per cubic centimeter; a melt index of 0.6 gram per 10 minutes; and a flow index of 50 grams per 10 minutes. This copolymer is treated in the same fashion as the above copolymers except that the primary antioxidant is 0.4 part by weight of vinyl modified polydimethylsiloxane; the secondary antioxidant is 0.75 part by weight of p-oriented styrenated diphenylamine; and the bimodal copolymer has an oscillating disk rheometer (5 degree arc at 360 degrees F) reading of 48 inch-pounds of torque.

- 10 -

COPOLYMERS F to I are monomodal copolymers of ethylene and an alpha-olefin (1-octene) made by the polymerization of the comonomers in the presence of metallocene single site catalyst systems. The melt indices and the densities are shown in the Table.

COPOLYMERS J and K are monomodal copolymers of ethylene and 1-hexene made by the polymerization of the comonomers in the presence of metallocene single site catalyst systems.

COPOLYMERS D and F to K are formulated in a similar manner to the other copolymers mentioned above.

Each resin formulation is tested for WTGR and the results compared with a control polyethylene homopolymer, which exhibits 100 percent WTGR. Each resin formulation is also tested for TREF. Variables and results are set forth in the following Table:

Table

Example	COPOLY-MER	MI (g/10 min)	Density (g/cc)	TREF (%)	WTGR (%)
1	A	0.6	0.923	25.1	3.6
2	B	1.0	0.910	26.2	0.7
3	C	4.0	0.905	12.2	5
4	D	4.0	0.905	23.2	10
5	E	0.6	0.913	14.9	2.3
6	F	5.0	0.870	1.2	68
7	G	3.5	0.910	less than 0.1	40
8	H	1.0	0.902	less than 0.1	81

- 11 -

9	I	1.0	0.870	1.1	179
10	J	1.7	0.923	2.1	258
11	K	2.5	0.908	1.8	172

In testing COPOLYMER E for (i) AC breakdown strength and (ii) dissipation factor, respectively, the results are (i) 83 percent retained AC breakdown strength after 21 days at 6 kilovolts at 1 kiloHertz for a 50 mil thick specimen and (ii) a very flat dissipation factor at less than 200 microradians for the entire temperature range of 23 to 95 degrees C.

The above results are confirmed by the extrusion coating of the above resin formulations on 14 AWG (American Wire Gauge) copper wires, and appropriate testing of the coated wires. The thickness of the coatings is 50 mils.

- 12 -

Claims

1. A cable comprising one or more electrical conductors or a core of one or more electrical conductors, each conductor or core being surrounded by a layer of insulation comprising a multimodal copolymer of ethylene and one or more alpha-olefins, each alpha-olefin having 3 to 8 carbon atoms, said copolymer having a broad comonomer distribution as measured by TREF with a value for the percent of copolymer, which elutes out at a temperature of greater than 90 degrees C, of greater than about 5 percent; a WTGR value of less than about 20 percent; a melt index in the range of about 0.1 to about 30 grams per 10 minutes; and a density in the range of 0.880 to 0.950 gram per cubic centimeter, and being prepared by a low pressure process.
2. The cable defined in claim 1 wherein the alpha-olefin is 1-butene, 1-hexene, 4-methyl-1-pentene, or 1-octene.
3. The cable defined in claim 1 wherein the copolymer has a TREF value greater than about 10 percent.
4. The cable defined in claim 1 wherein the copolymer has a WTGR value less than about 10 percent.
5. The cable defined in claim 1 wherein the copolymer has a density in the range of about 0.880 to about 0.930 gram per cubic centimeter.
6. The cable defined in claim 1 wherein the copolymer has a melt index in the range of about 0.5 to about 10 grams per cubic centimeter.

INTERNATIONAL SEARCH REPORT

Int. Appl. No.

PCT/US 97/10374

A. CLASSIFICATION OF SUBJECT MATTER
 IPC 6 H01B7/28 H01B3/44

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
 IPC 6 H01B

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	EP 0 735 545 A (UNION CARBIDE) 2 October 1996 see the whole document ---	1-6
A	EP 0 410 431 A (UNION CARBIDE) 30 January 1991 see the whole document ---	1-6
A	DATABASE WPI Section Ch, Week 9204 Derwent Publications Ltd., London, GB; Class A18, AN 92-029103 XP002040028 & JP 03 276 515 A (HITACHI CABLE LTD) , 6 December 1991 see abstract --- -/--	1-6

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents :

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *Z* document member of the same patent family

Date of the actual completion of the international search

8 September 1997

Date of mailing of the international search report

30.09.97

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
 NL - 2280 HV Rijswijk
 Tel. (+ 31-70) 340-2040, Tx. 31 651 epo nl,
 Fax (+ 31-70) 340-3016

Authorized officer

Drouot, M-C

INTERNATIONAL SEARCH REPORT

Pat. Application No

PCT/US 97/10374

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A,P	<p>DATABASE WPI Section Ch, Week 9648 Derwent Publications Ltd., London, GB; Class A17, AN 96-477457 XP002040029 & AU 50382 96 A (UNION CARBIDE CHEM & PLASTICS TECHNOLOGY) , 10 October 1996 see abstract</p> <p>-----</p>	1-6

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/US 97/10374

Patent document cited in search report	Publication date	Patent family member(s)	Publication date
EP 735545 A	02-10-96	CA 2173038 A	01-10-96
EP 410431 A	30-01-91	AT 122815 T	15-06-95
		AU 636900 B	13-05-93
		AU 5977290 A	31-01-91
		CA 2022312 A	27-01-91
		CN 1050728 A	17-04-91
		DE 69019429 D	22-06-95
		DE 69019429 T	14-09-95
		ES 2071709 T	01-07-95
		JP 3066736 A	22-03-91
		JP 8019291 B	28-02-96